



Production of Sustainable aircraft grade Kerosene from water and air powered by Renewable Electricity, through the splitting of CO₂, syngas formation and Fischer - Tropsch synthesis

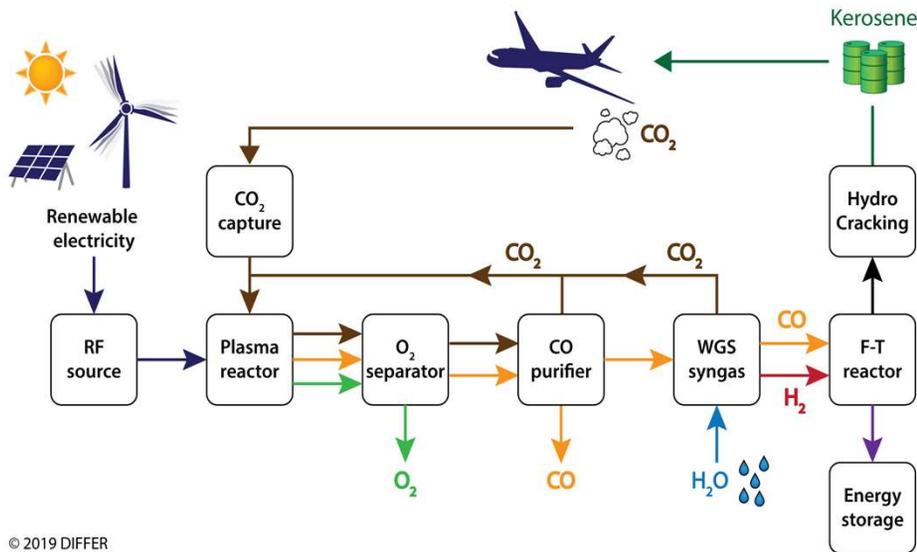
KEROGREEN - A plasma-based approach for CO₂ neutral fuel production

S. Welzel, A. Pandiyan, V. Kyriakou, D. Neagu, R. Sharma, F. Peeters, B. Wolf, W. Bongers,
M.C.M. van de Sanden, A. Goede, M. Tsampas

DUTCH INSTITUTE FOR FUNDAMENTAL ENERGY RESEARCH, EINDHOVEN, THE NETHERLANDS



Kerogreen project



KIT / Energy Lab (www.elab2.kit.edu)



Kerogreen aim: Demonstration of the full chain process from renewable electricity, CO₂ (captured) and H₂O to kerosene.

- Research and optimization of individual process steps TRL (1-3) → 4
- Integration phase at Karlsruhe Institute of Technology → 3 L per day
- Duration 2018-2022



IK
INERATEC



This project has received funding from the European Union's Horizon 2020 Research and Innovation Programme under GA-Nr. 763909

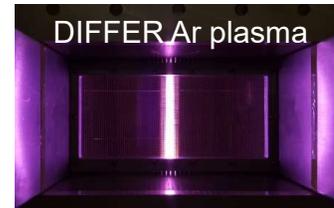


Outline

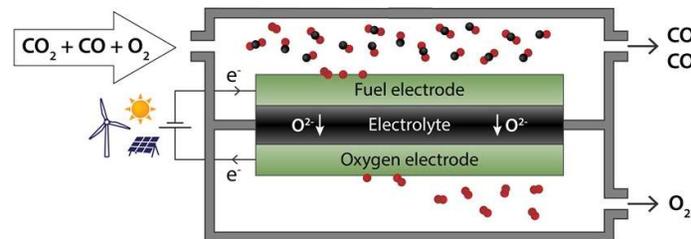
- Kerogreen project



- Plasmolysis of CO₂



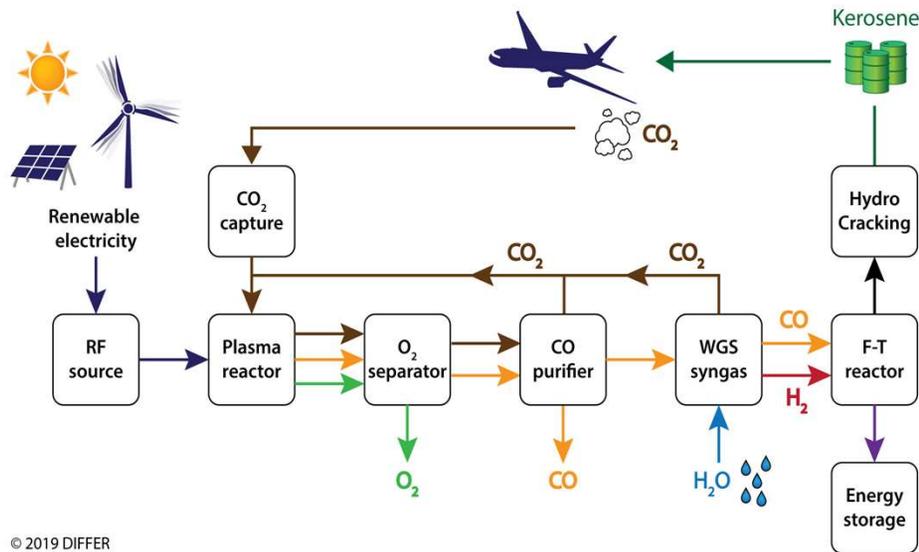
- Oxygen separation by means of Solid oxide electrolyte cells (SOECs)



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Kerogreen project



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KEROGREEN offers an innovative conversion route based on plasma driven dissociation of CO₂, separation of oxygen by means of solid oxide electrolyte cells and Fischer-Tropsch (F-T) synthesis of kerosene.

- CO₂ plasmolysis (DIFFER)
- O₂ separation (DIFFER, VITO, Cerpotech, Hygear)
- CO purification (HYGEAR)
- Water gas shift reaction reaction (KIT)
- F-T synthesis (INERATEC)
- Heavy HC hydrocracking (KIT)

Main challenges

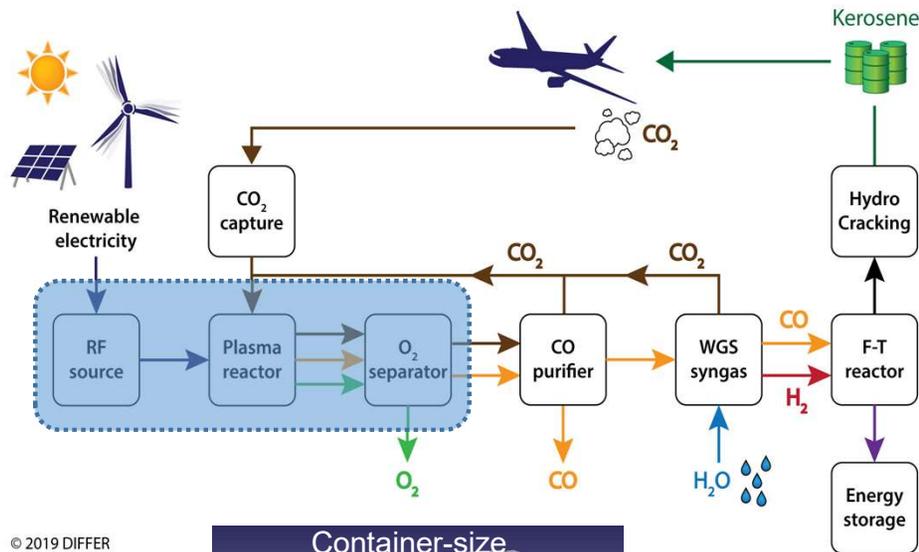
- Oxygen separation after plasmolysis by SOEC
- System integration of different technologies into one container sized assembly
- Maximization of the energy and carbon efficiency of the full chain



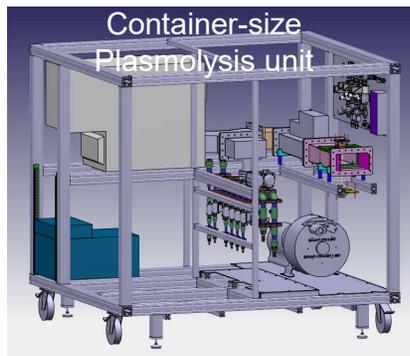
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Kerogreen project

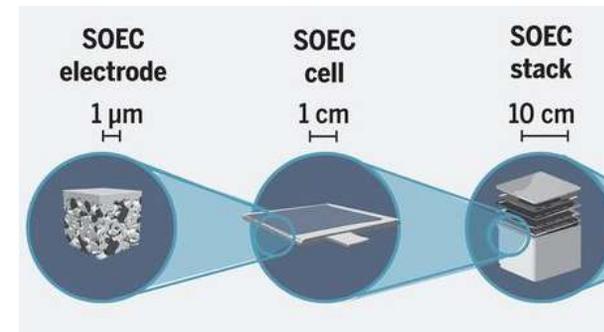


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DIFFER involvement

- Plasma modeling and optimization for process chain
- Plasma upscaling from 1 to 6 kW
- Material requirements for using SOEC as oxygen separator
- SOEC upscaling from 1W to 1.5 kW



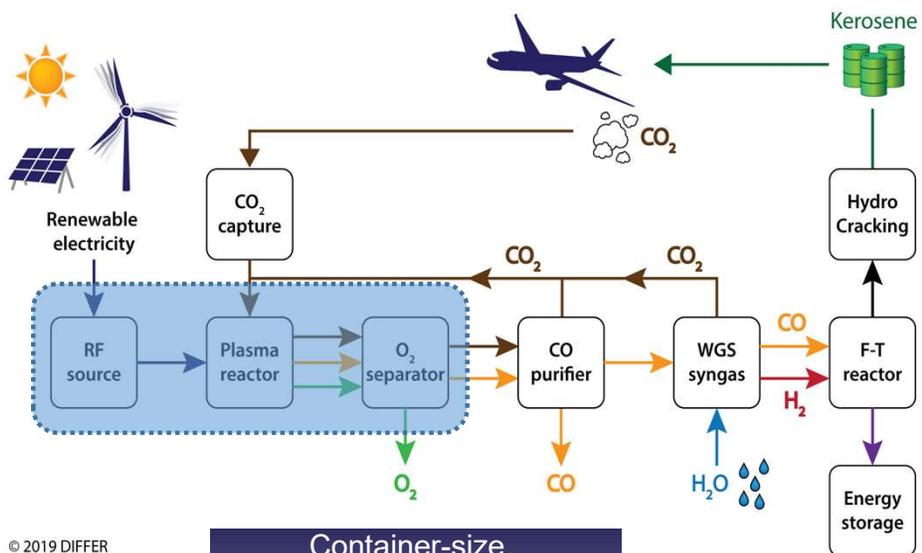
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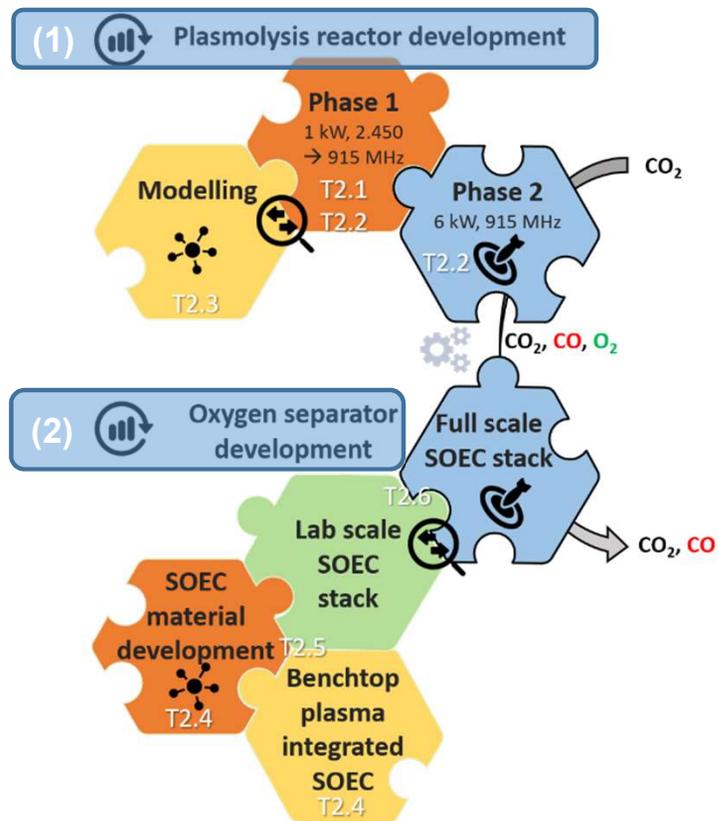
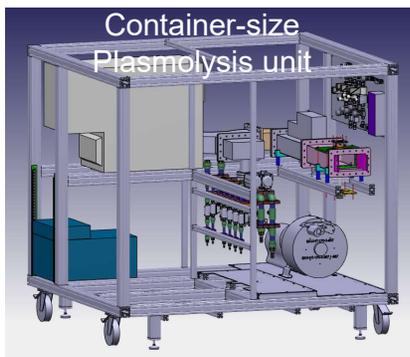
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Kerogreen project



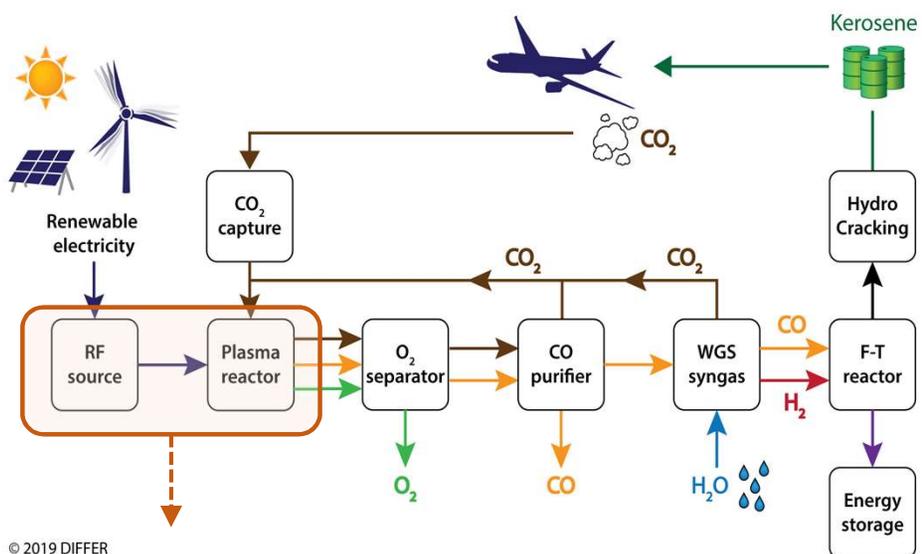
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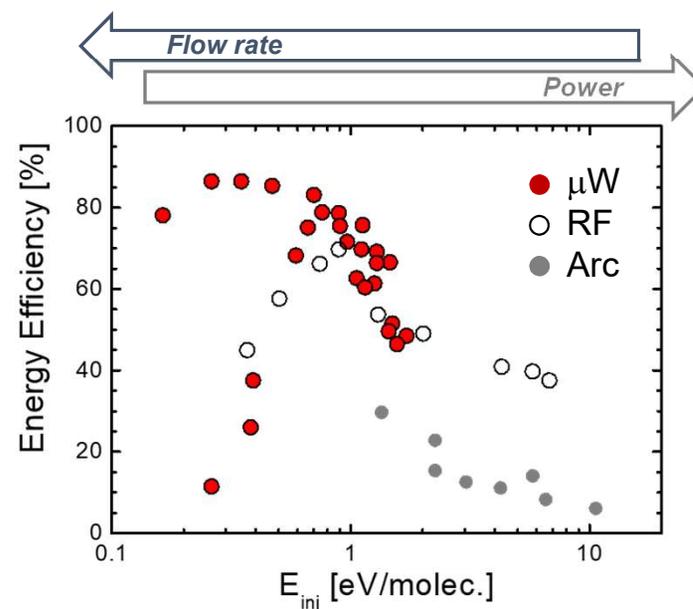
CO₂ plasmolysis: Why?



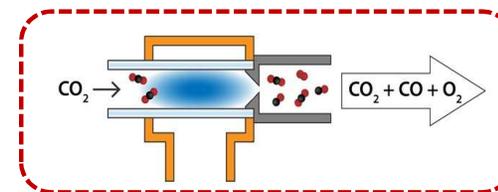
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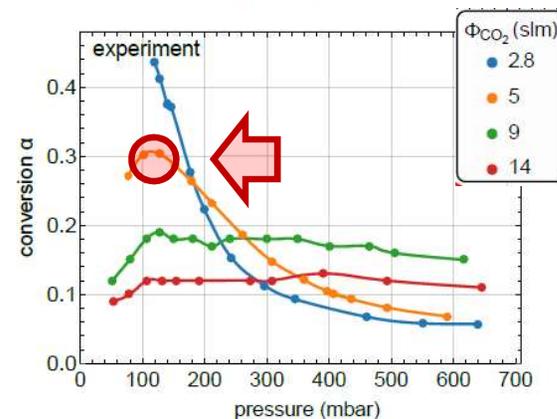
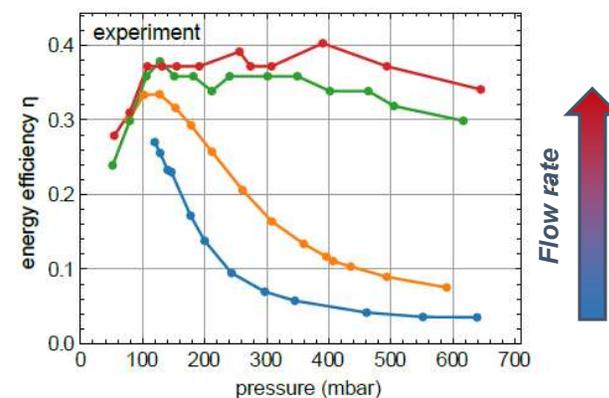
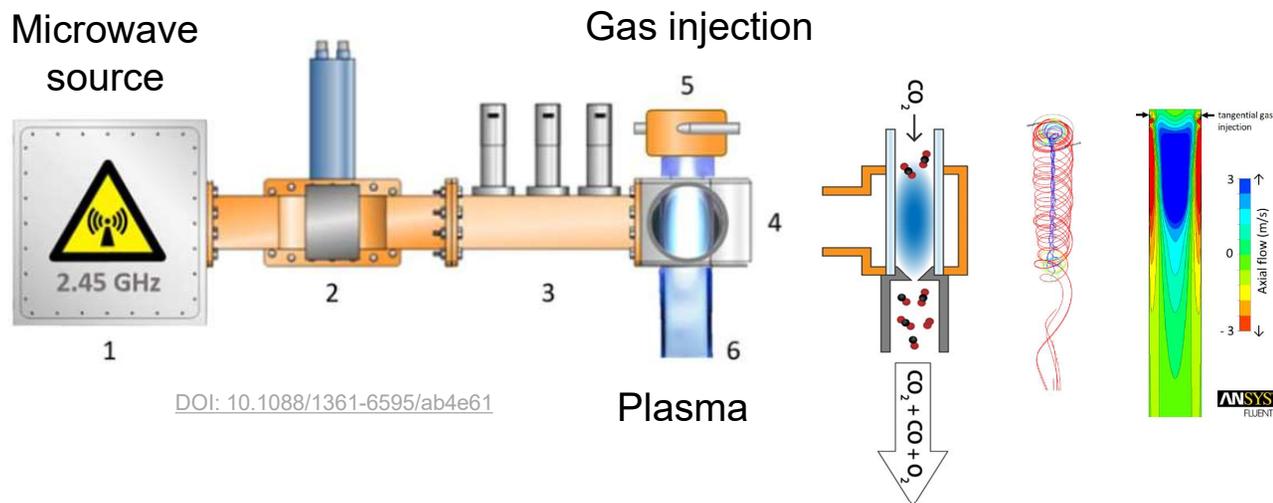
- Input: CO₂ + renewable electricity
- Output: CO₂, CO and O₂
- High energy efficiency, ...
- Main challenge O₂ separation



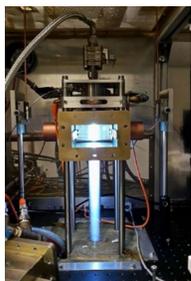
DOI: 10.1017/CBO9780511546075



CO₂ plasmolysis: How?



- Conversion & efficiency interdependent (complex!)
- Different discharge modes
- Gas temperatures $\gg 1000$ K



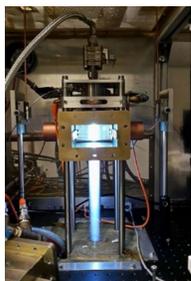
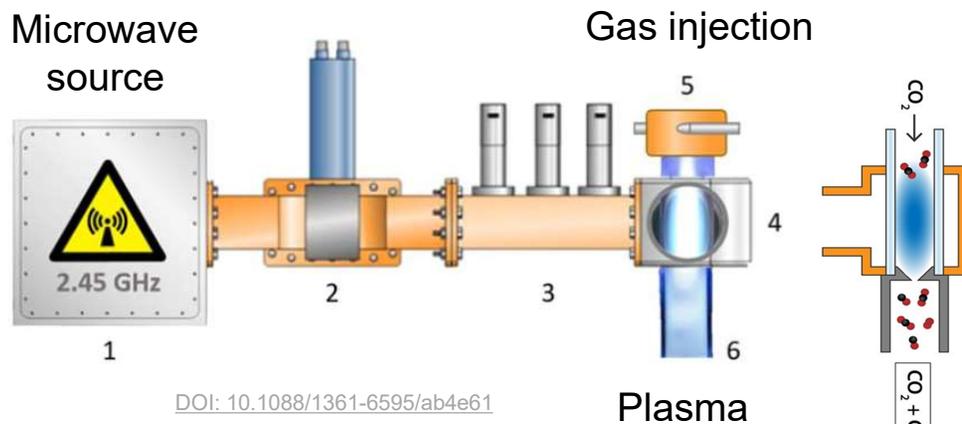
A.J. Wolf et al. The J. of Physical Chemistry C, 124 (2020) 16806



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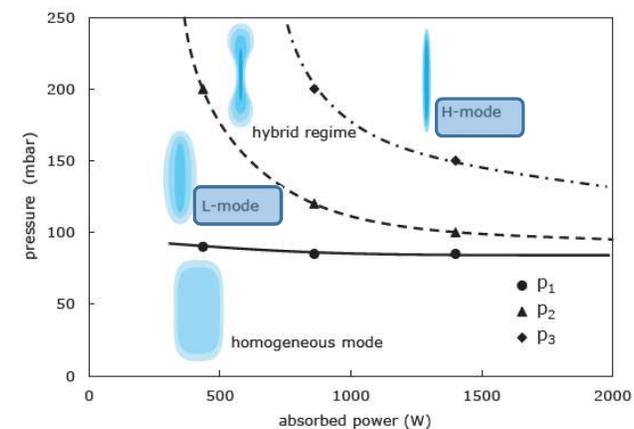
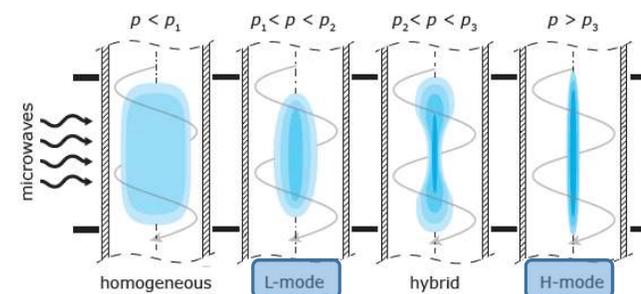


CO₂ plasmolysis: How?

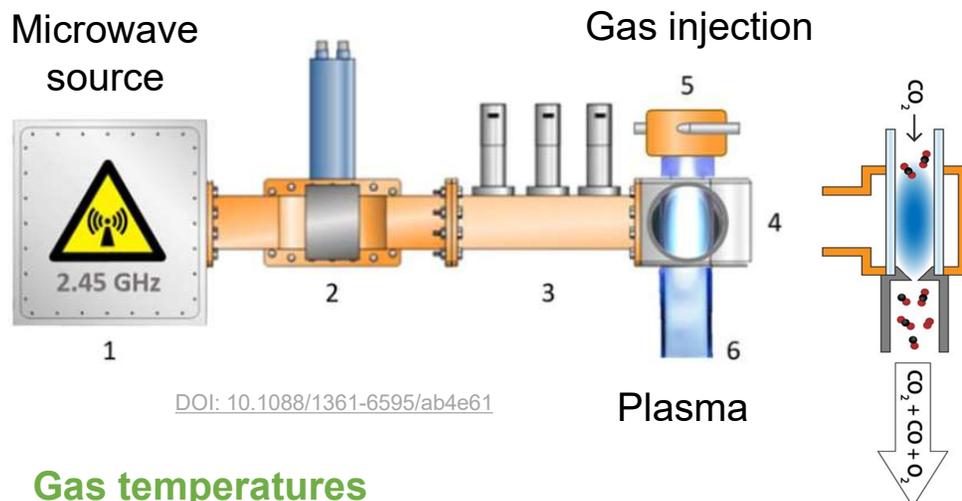


- Conversion & efficiency interdependent (complex!)
- Different discharge modes
- Gas temperatures $\gg 1000$ K

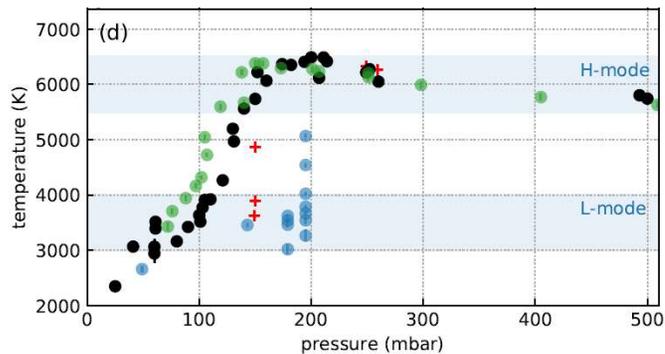
Discharge modes



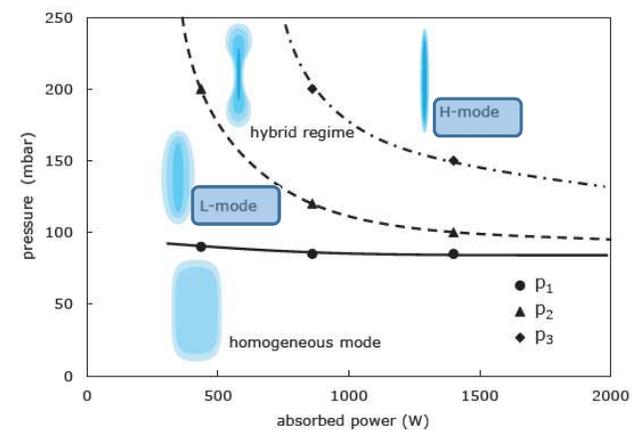
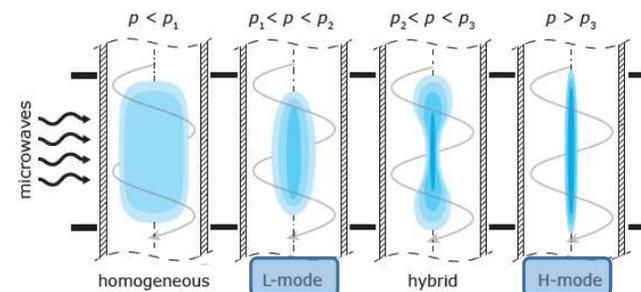
CO₂ plasmolysis: How?



Gas temperatures



Discharge modes



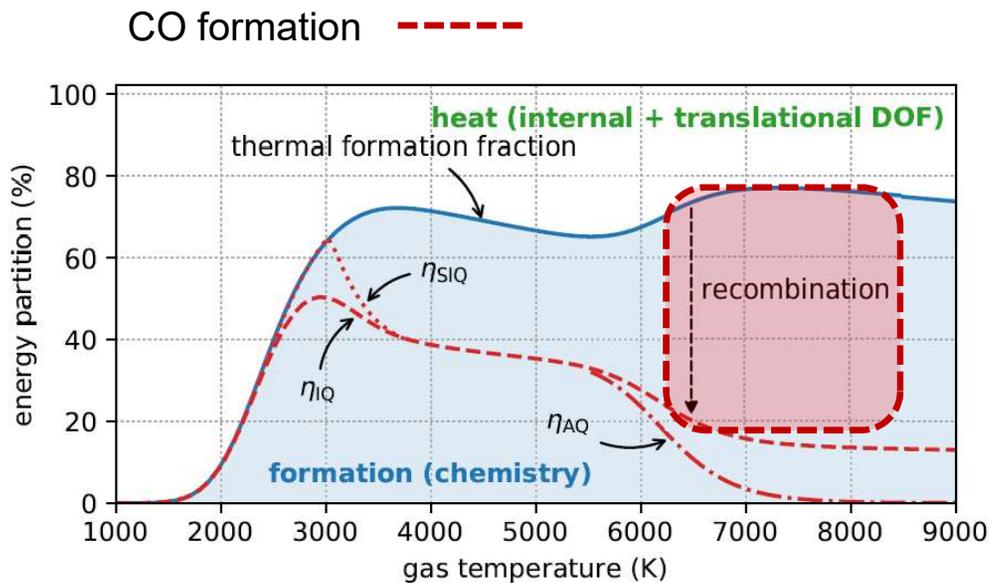
A.J. Wolf et al. Plasma Sources Sci. Techn., 29 (2020) 025005



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CO₂ plasmolysis: Challenges & Take away (I)



A.J. Wolf et al. The J. of Physical Chemistry C, 124 (2020) 16806

Gas temperature

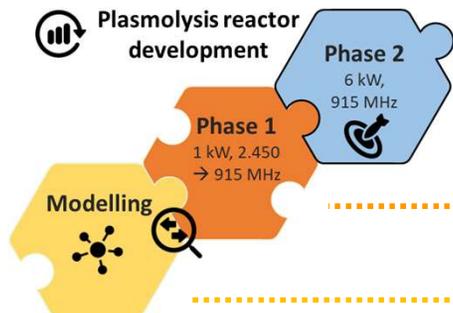
- Processes & efficiency determined by gas temperature
- Gas temperature cannot be set
- Pressure determines discharge mode (and T)
- $T \gg 1000$ K (material challenge !)

CO yield

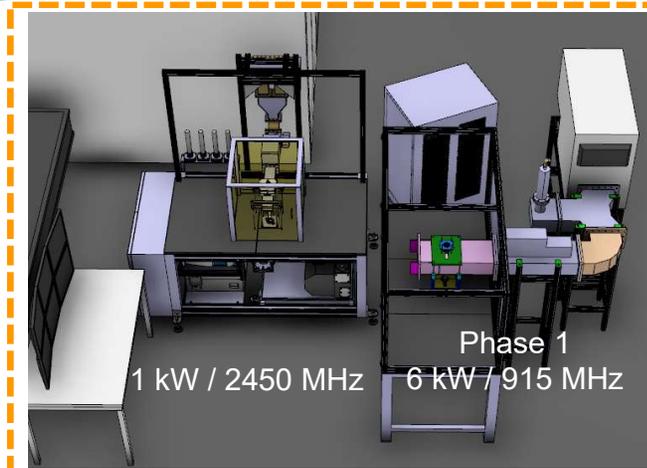
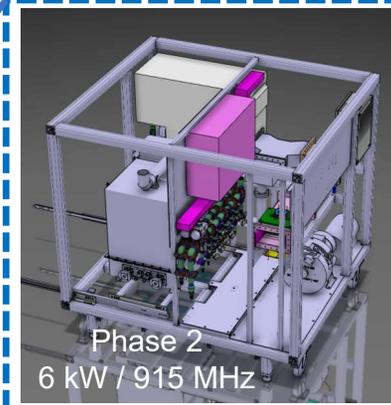
- CO yield determined by recombination
- Final CO yield depends of the way of extraction
- Flow pattern = recirculation zones
 - Quick expansion (pumping required ☹)
 - Fast, significant cooling (quenching, Q) (material + surface area challenge)



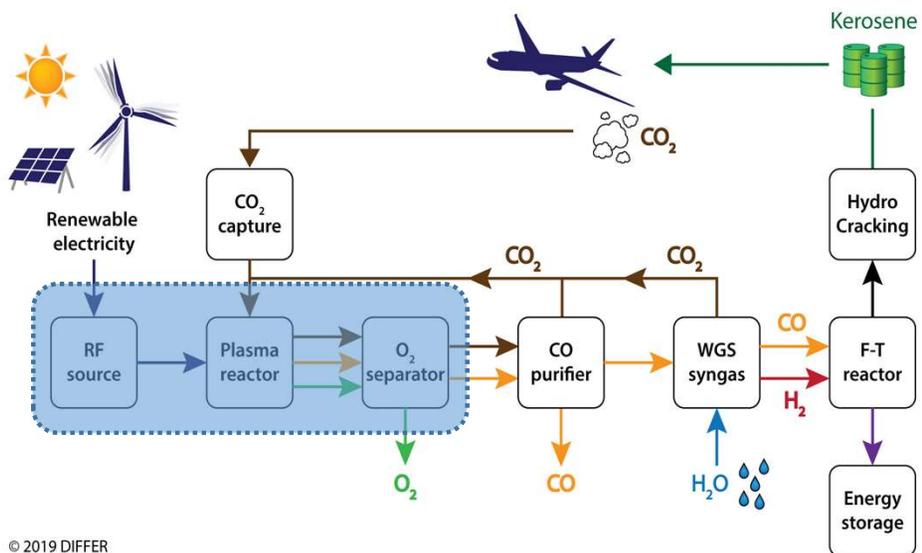
CO₂ plasmolysis: Scale up



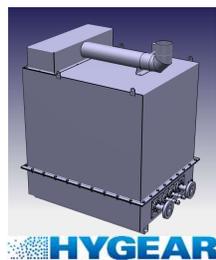
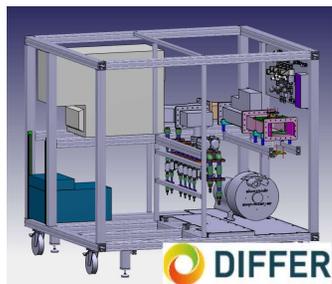
	Power [kW]	Frequency [MHz]	Scale
Phase 2	6	915	Container/Module
Phase 1	6	915	Lab
(InitSF)	1-2	2450	Lab



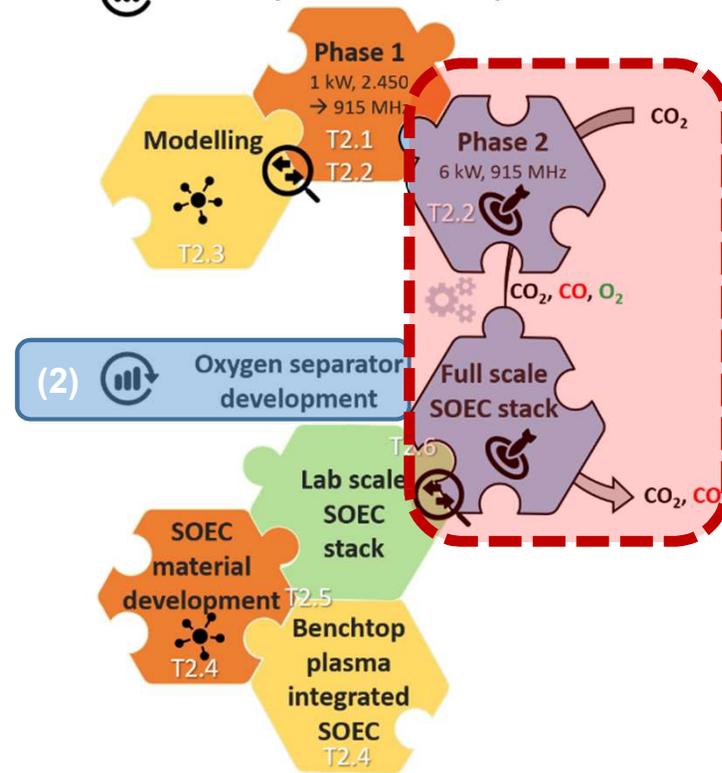
Kerogreen project: Merging Technologies



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Plasmolysis reactor development



(2) Oxygen separator development



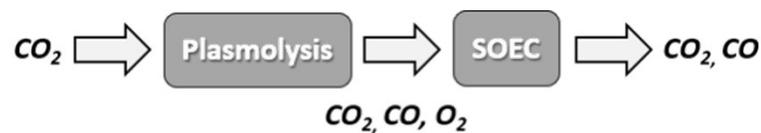
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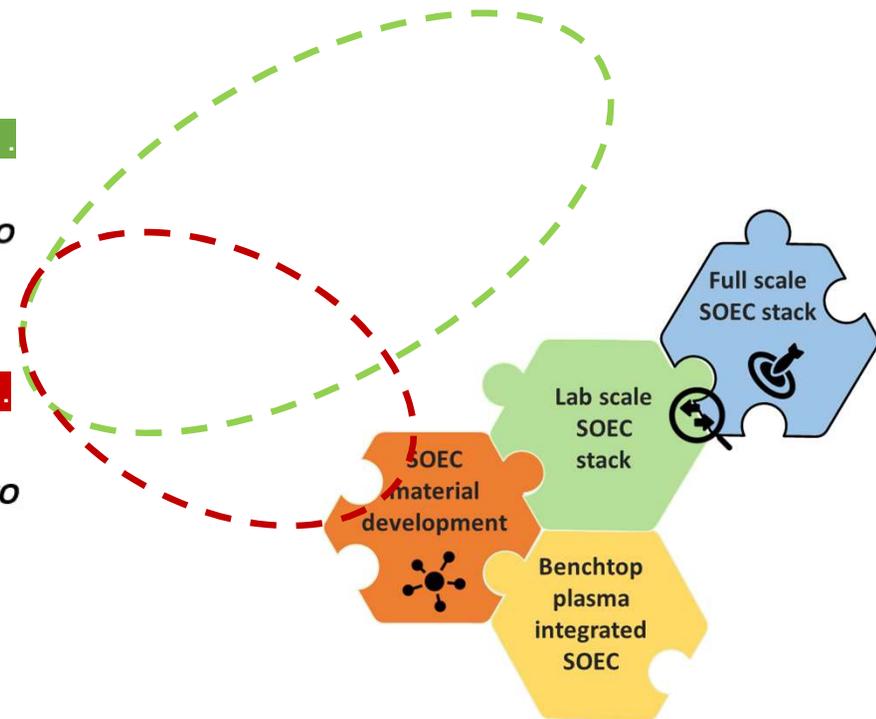
Kerogreen project: Oxygen separation

- Oxygen separation by solid-oxide electrolyte cells (SOECs)
- Approaches

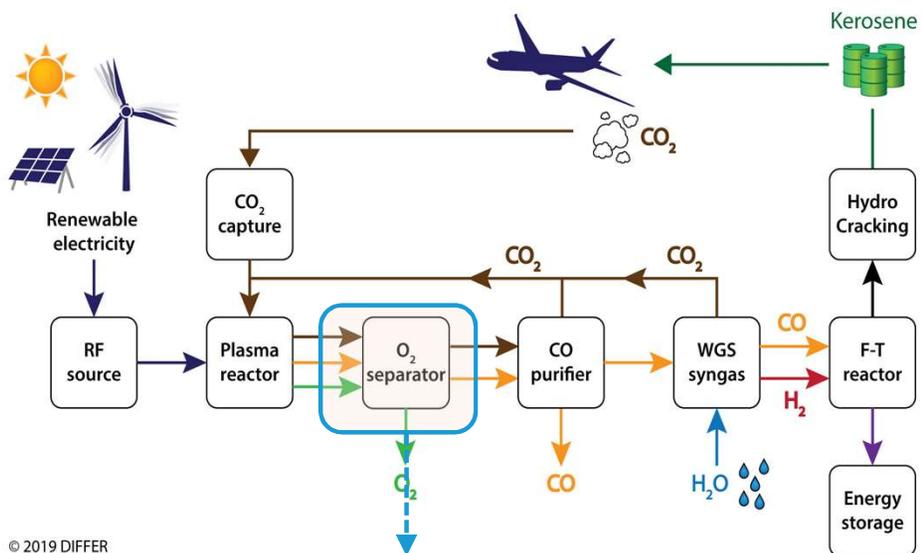
- **Downstream (!)**



- **Plasma-integrated**



SOEC as oxygen separator

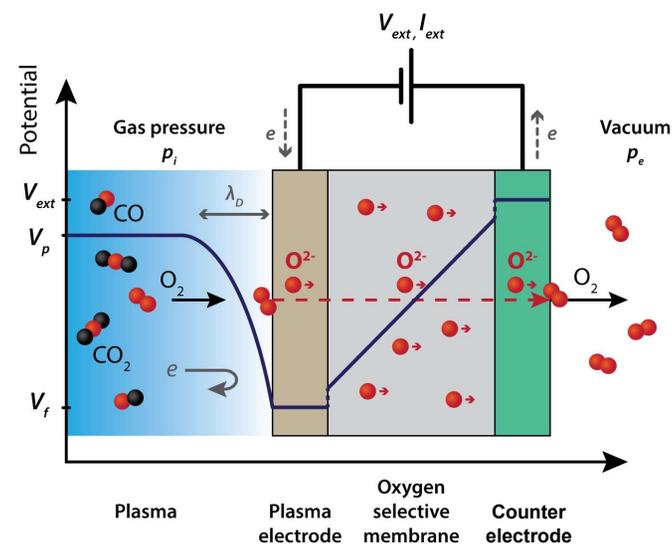


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O₂ separation

- Difficult process
- Lack of literature
- SOEC: Electrochemical O₂ pumping



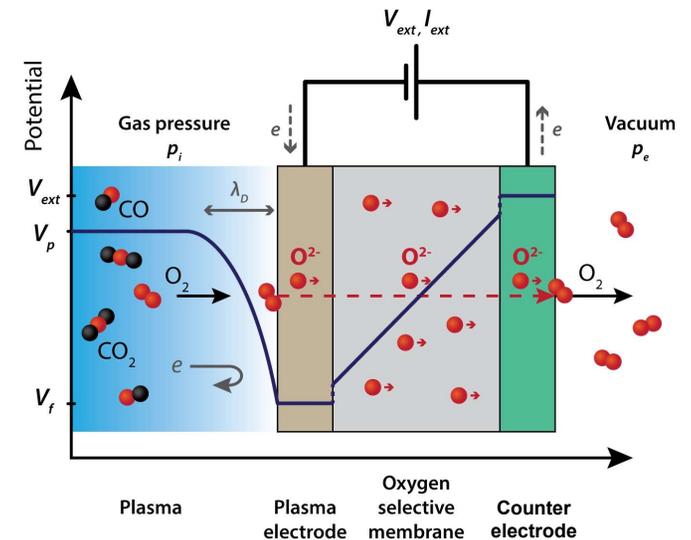
Plasma electrode reactions

- $O_2 + 4e^- \rightarrow 2O^{2-}$ (desired)
- $CO_2 + 2e^- \rightarrow CO + O^{2-}$ (neutral)
- $2CO + O_2 \rightarrow 2CO_2$ (unwanted)

SOEC as oxygen separator

Functionalities

- **For both electrodes:**
Mixed electronic & ionic conductivity
Low overpotential losses (gas composition, T)
- **Plasma electrode**
Unconventional mixture (CO₂ / CO / O₂)
Poor CO activity
- **Electrolyte**
Oxygen ion conductivity
Low resistance → thin
- **Overall**
High oxygen fluxes
Stability

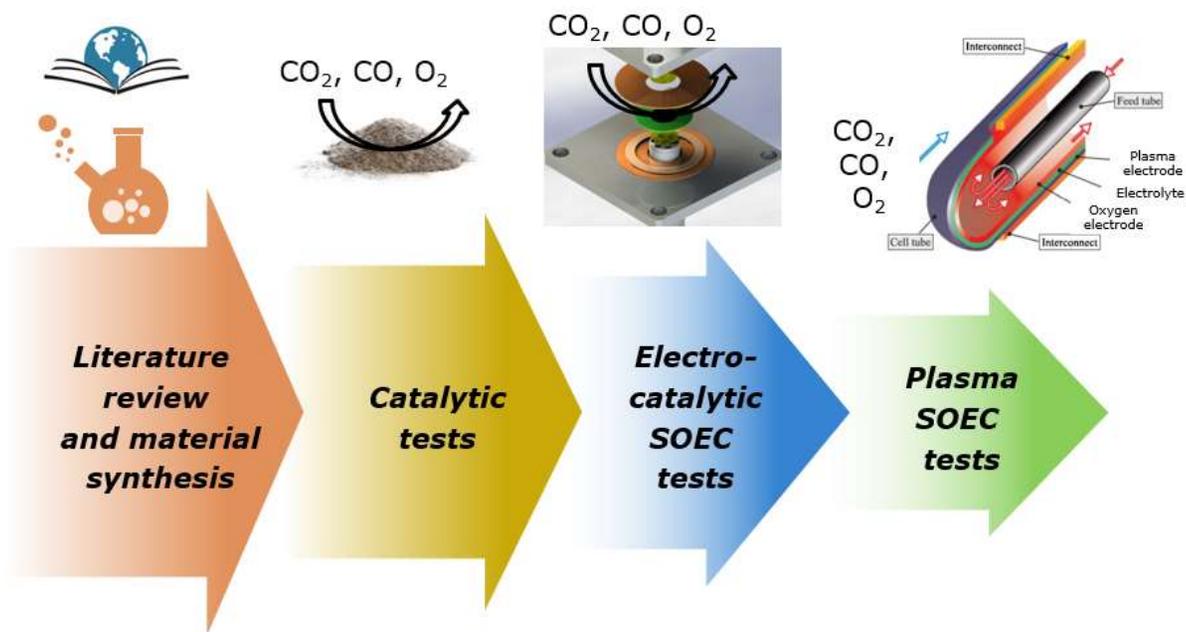


Plasma electrode reactions

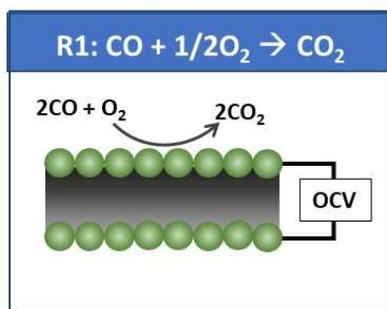
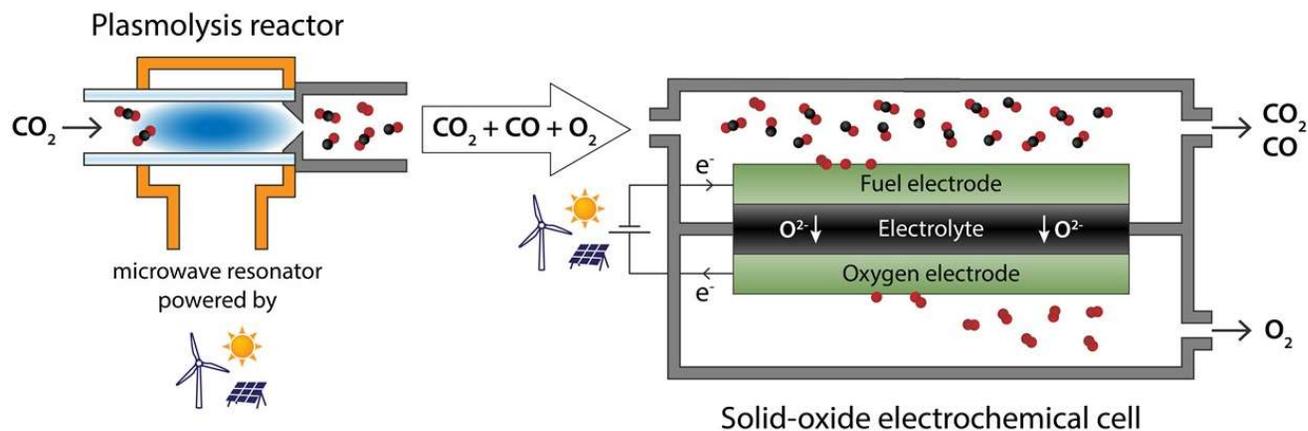
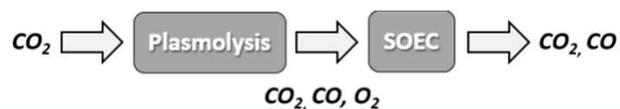
- $O_2 + 4e^- \rightarrow 2O^{2-}$ (desired)
- $CO_2 + 2e^- \rightarrow CO + O^{2-}$ (neutral)
- $2CO + O_2 \rightarrow 2CO_2$ (unwanted)

Plasma electrode development

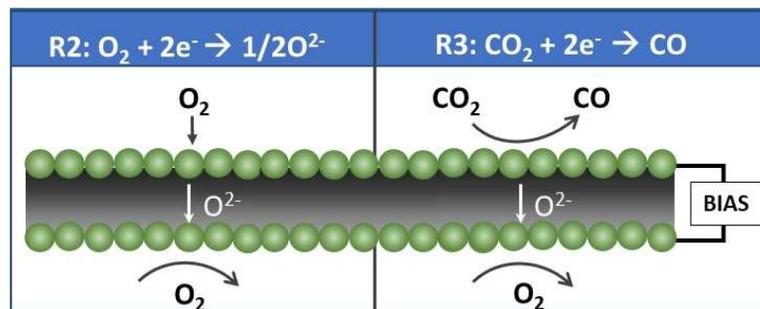
- Literature review
- Material synthesis  Cerpotech
- Catalytic tests
- SOEC electrocatalytic tests
- Plasma SOEC integrated tests



Possible reactions



Unwanted



Desired

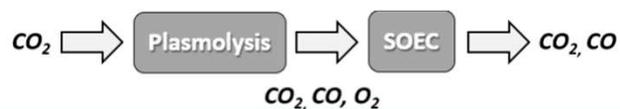
Neutral



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Electrochemical characterization

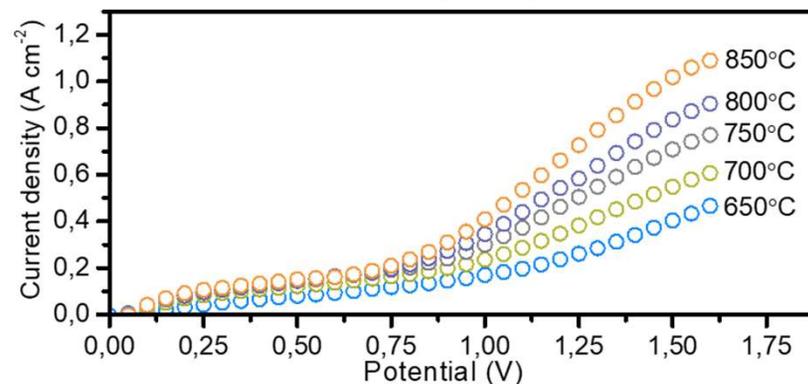
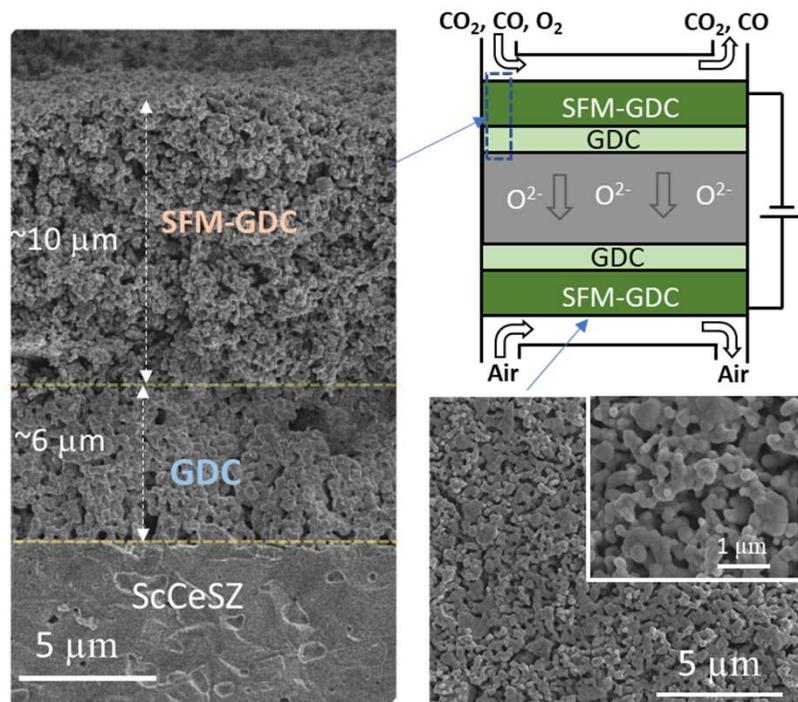


SFM: $Sr_2Fe_{1.5}Mo_{0.5}O_{6-\delta}$

CO_2 plasmolysis equivalent gas mixture

DOI: 10.1016/j.ijhydene.2010.08.016

○ 650°C
 ○ 700°C
 ○ 750°C
 ○ 800°C
 ○ 850°C



A. Pandiyan et al. (in preparation)

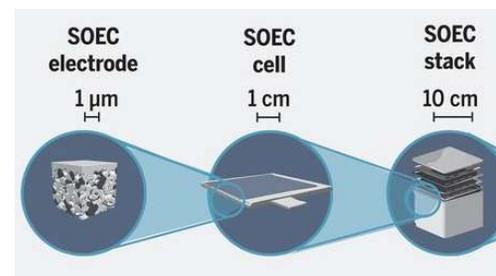
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Oxygen separation: Challenges & Take away (II)

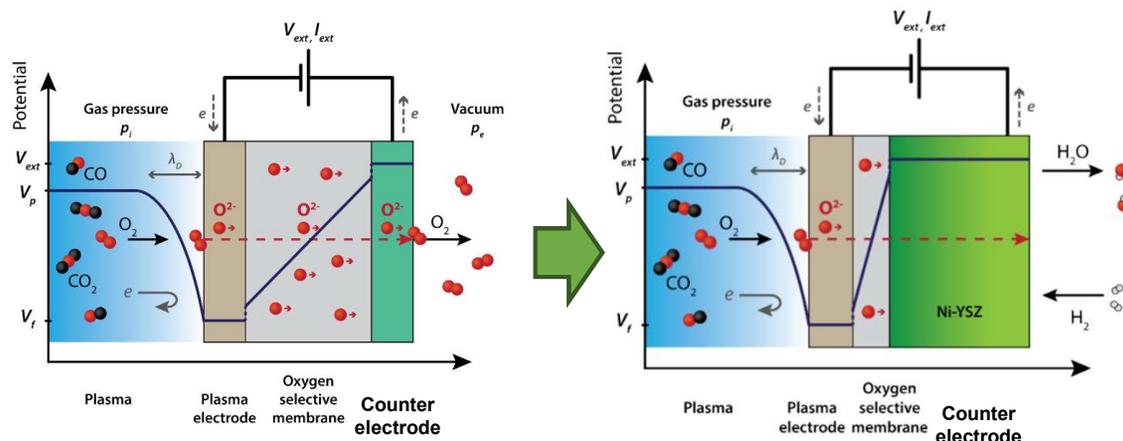
Cell level

- Oxygen separation from CO₂ plasmolysis equivalent mixtures has been demonstrated on cell level.
- SOEC operation with CO₂ plasmolysis equivalent mixtures improves materials stability.
- Limited choice of (commercially available) materials (material challenge!)
- Plasma-integrated approach being developed at DIFFER (TRL 1!)



Stack level & KEROGREEN chain integration

- Advanced SOEC architectures will decrease ohmic losses:
 - allow operation at lower T (less CO losses),
 - while preserving high oxygen pumping rates.
- KEROGREEN: Commercial SOFC vendor → 1.5 kW unit (incl. H₂ co-electrolysis)





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