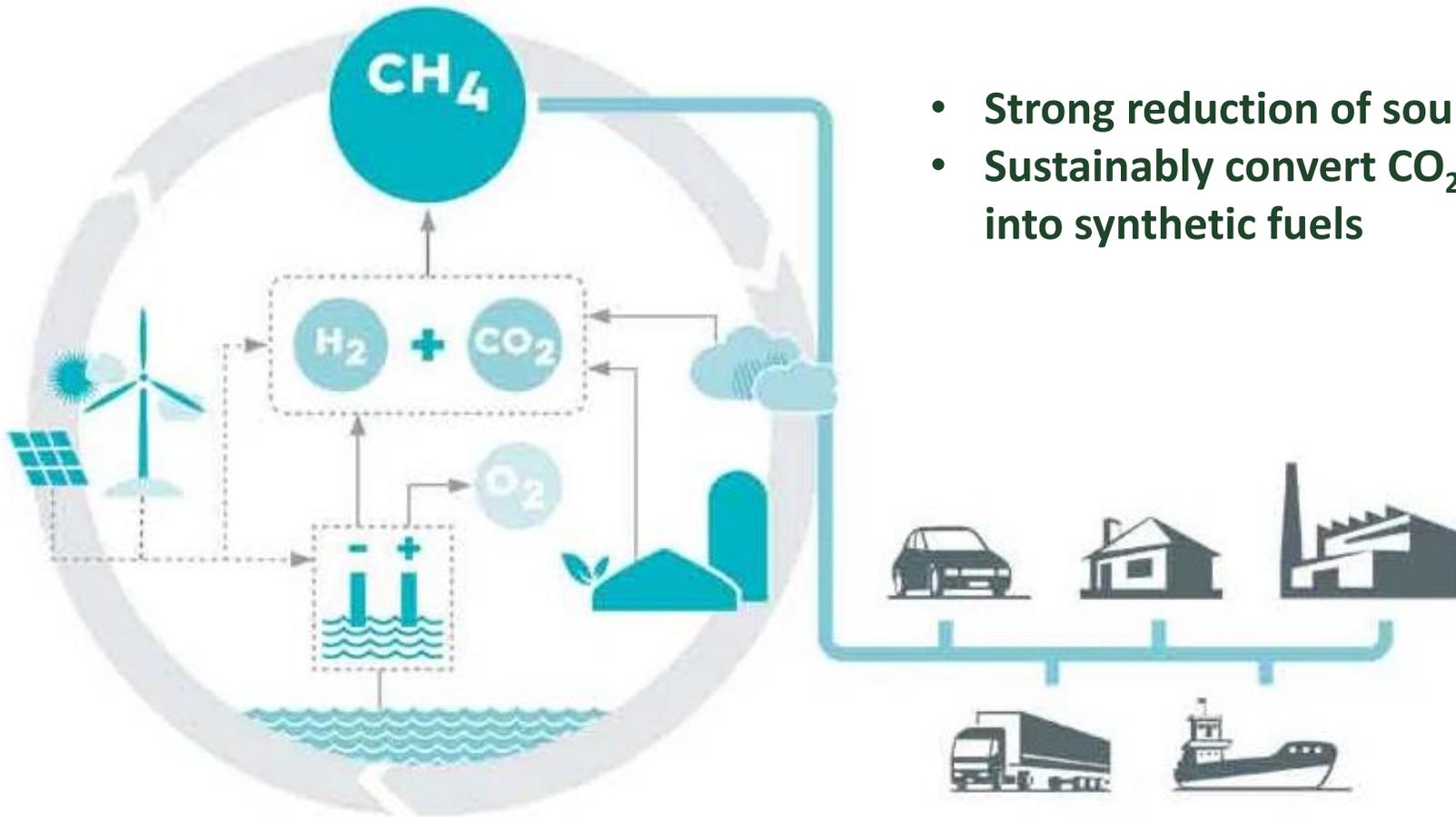




## Combined CO<sub>2</sub> Capture & Methanation

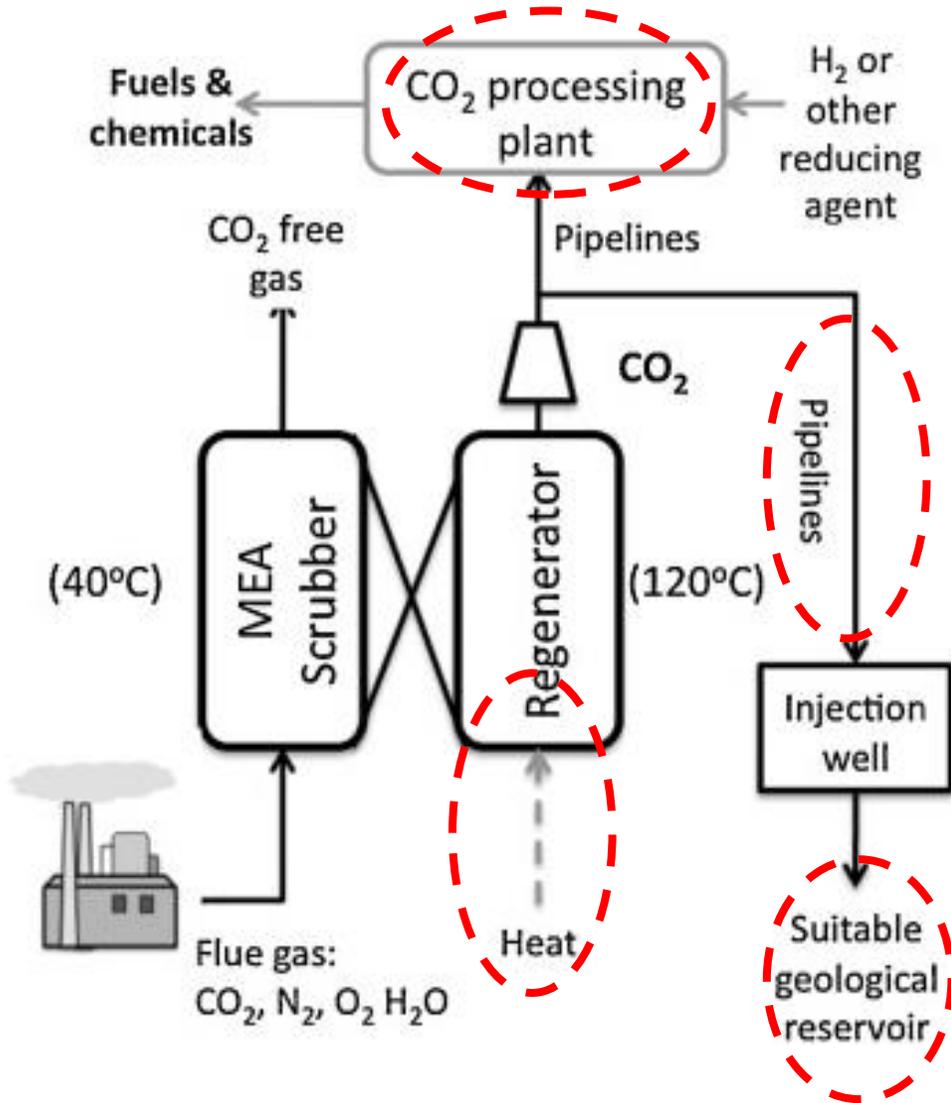
# CO<sub>2</sub> Capture & Utilization – Power to Gas



- **Strong reduction of source greenhouse gas emissions**
- **Sustainably convert CO<sub>2</sub> emissions from industrial processes into synthetic fuels**

- CO<sub>2</sub> capture from point sources or air
- H<sub>2</sub> from renewable energy sources
- Carbon neutral cycle
- Chemical storage of excess energy
- CH<sub>4</sub> (SNG) advantageous energy carrier: easily handled, existing distribution grid

# Conventional CO<sub>2</sub> Capture, Utilization & Storage



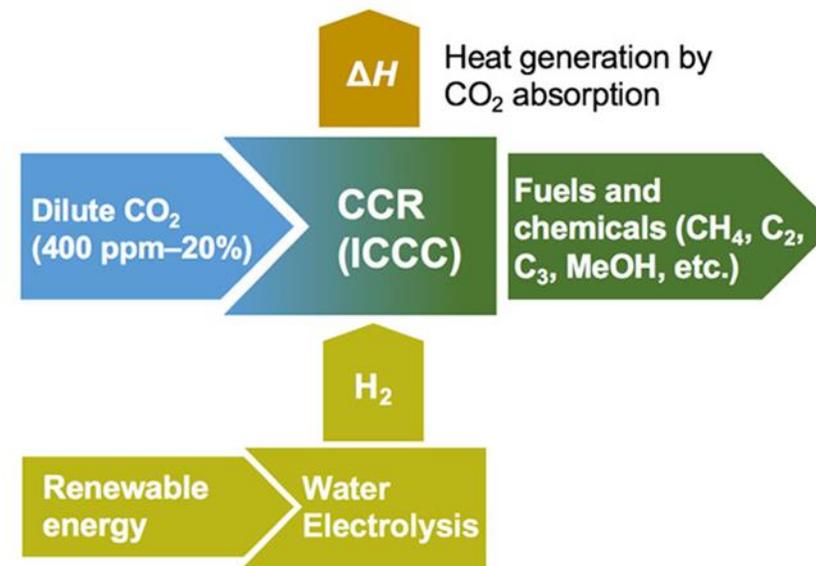
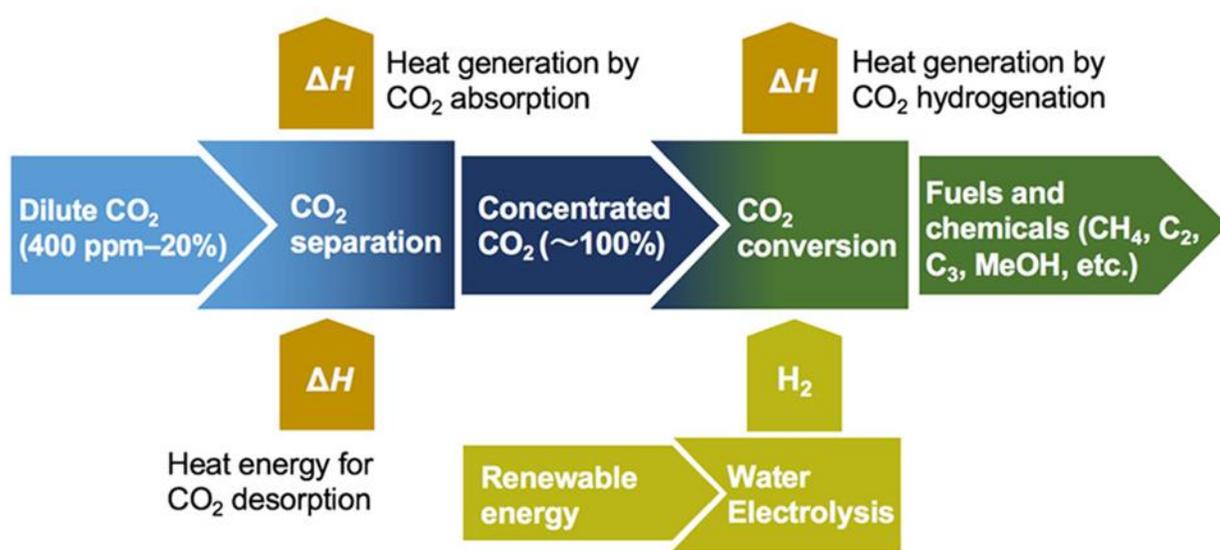
	Absorption	Adsorption	Membrane
Energy requirement	4-6 MJ/kg CO <sub>2</sub>	2-3 MJ/kg CO <sub>2</sub>	0.5-6 MJ/kg CO <sub>2</sub>
Cost	expensive	expensive	expensive
CO <sub>2</sub> recovery	90-98%	80-95%	80-90%
Challenges	<ul style="list-style-type: none"> <li>Corrosion</li> <li>Huge energy req.</li> <li>Solvent degradation</li> </ul>	<ul style="list-style-type: none"> <li>Attrition</li> <li>Pressure drops</li> <li>Affected by impurities</li> </ul>	<ul style="list-style-type: none"> <li>Not suitable for high T</li> <li>Low CO<sub>2</sub> select.</li> <li>Costly membranes</li> </ul>

Omodolor, et al. Ind. Eng. Chem. Res. 2020, 59, 17612–17631.

- energy intensive CO<sub>2</sub> desorption step: high cost
- problem of transporting concentrated CO<sub>2</sub> to another site for storage or utilization
- Difficult thermal management of methanator

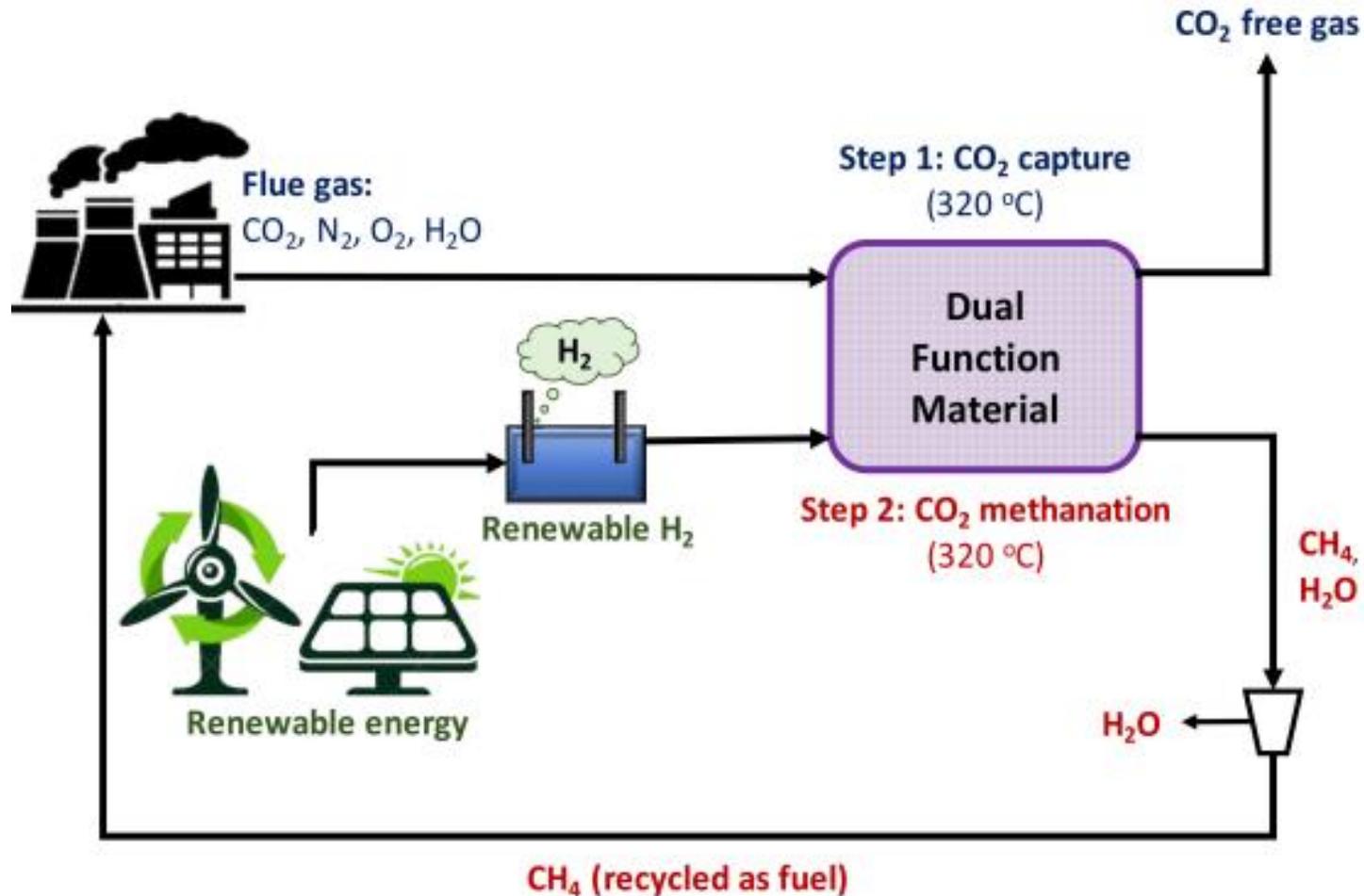
# Can we make it simpler ?

## Combined CO<sub>2</sub> Capture & Methanation

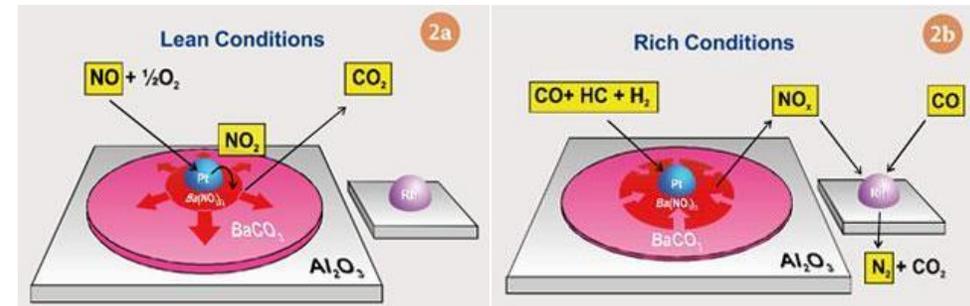


- Innovative strategy integrating both technologies
- No need for CO<sub>2</sub> desorption and transport

# Combined CO<sub>2</sub> Capture & Methanation



- **Dual Function Materials** capture CO<sub>2</sub> from industrial flue gases (or even air) and release it as concentrated synthetic natural gas (SNG)
- **Catalytic looping process**
- 2 half-cycles with a CO<sub>2</sub> sorbent/catalyst
- Requires materials / processes to switch between capture & methanation cyclically
- Analogy with LNT deNO<sub>x</sub>

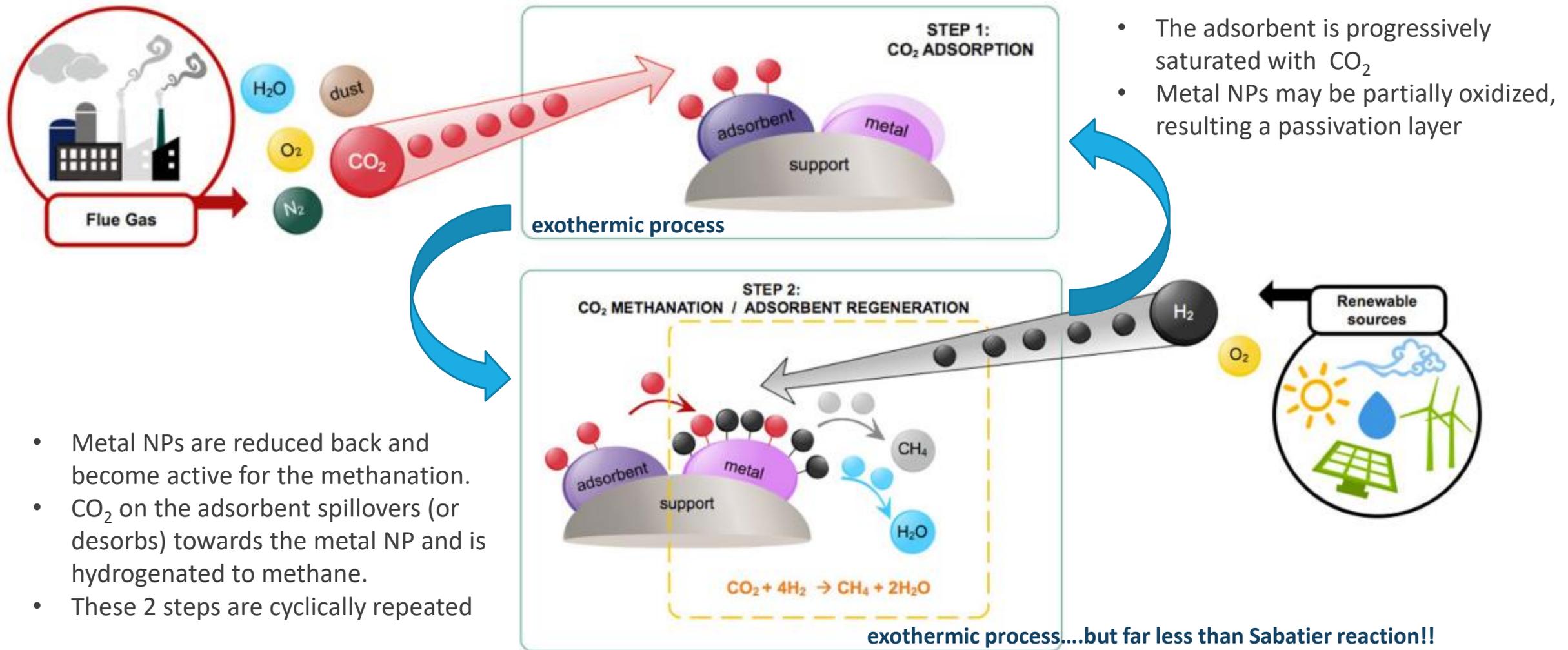


Tsiotsias, et al. Catalysts 2020, 10, 1–36; 1

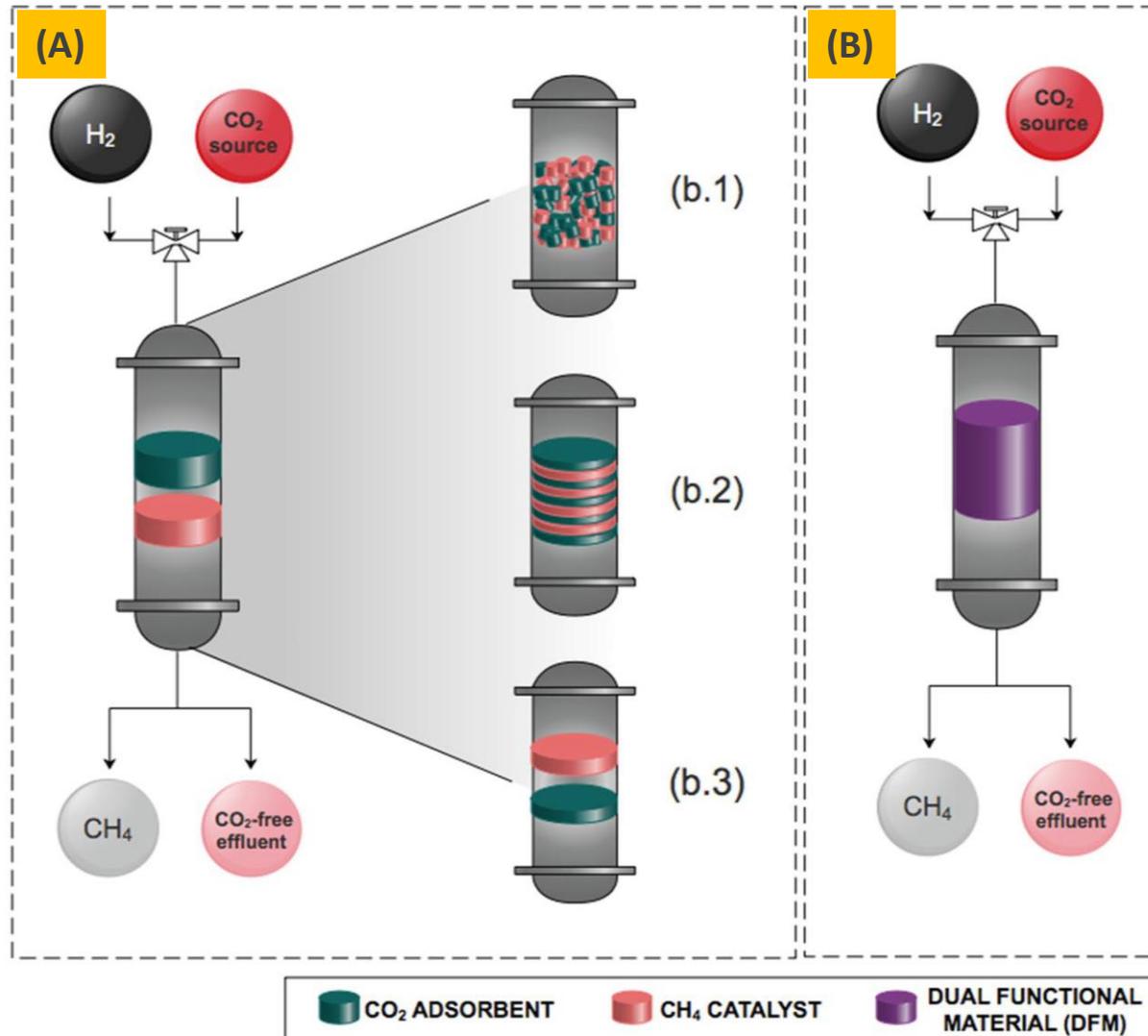
Arellano-Treviño, et al. Chem. Eng. J. 2019, 375, 121953

Bermejo-López et al. Appl. Catal. B Environ. 2019, 256, 117845.

# Combined CO<sub>2</sub> Capture & Methanation



# Combined CO<sub>2</sub> Capture & Methanation



## Proposed process configurations

### A. Mixed Beds of Sorbent + Catalyst

- Thermal coupling: heat of methanation drives CO<sub>2</sub> desorption / sorbent regeneration

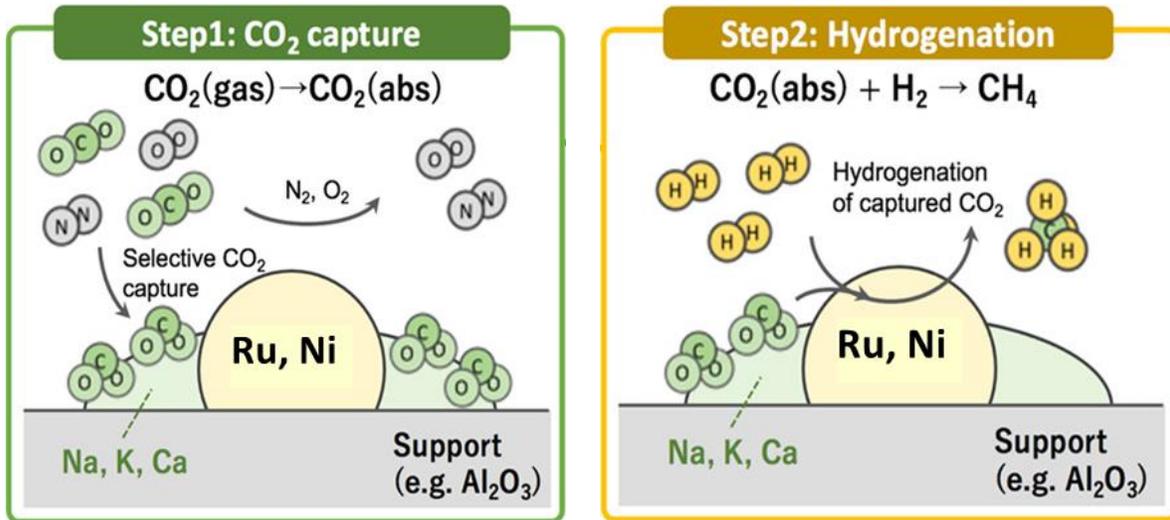
### B. DFM: Intimate mix at nanoscale

- ✓ Thermal + Chemical coupling via spill-over from sorbent to catalyst
- ✓ More effective regeneration at lower temperatures
- ✓ Higher CH<sub>4</sub> productivity

# Key to success: development of highly effective DFMs

## State of the art DFMs:

- Active phase: 5-10 % wt. Ru
- Sorbent: 5-15% Na (K, Ca)
- Support:  $\text{Al}_2\text{O}_3$



## What can we improve?

- ✓ Catalytic methanation activity (work @ lower temperature)
- ✓ CH<sub>4</sub> selectivity
- ✓ Cost (metal loading)
- ✓ Oxidation resistance
- ✓ Lower parasitic H<sub>2</sub> consumption
- ✓ Large & fast CO<sub>2</sub> capture capacity + selectivity
- ✓ Fast & easy regeneration @ low temperature
- ✓ Mechanical strength
- ✓ Stability / Durability / Tolerance to Poisoning

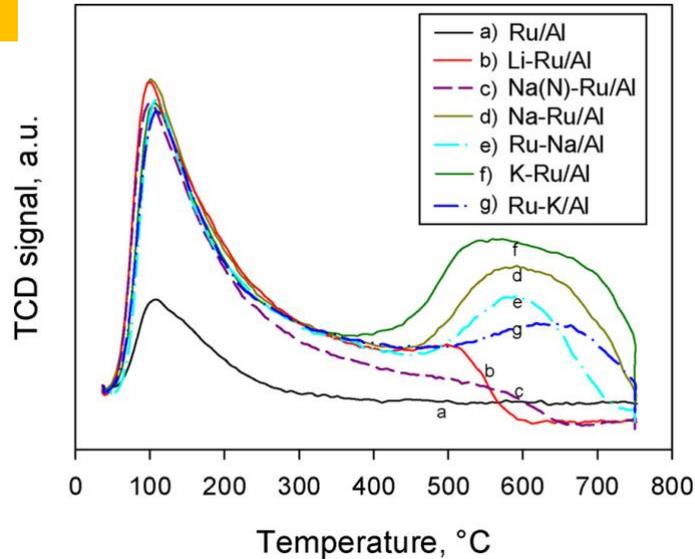
# Key to success: DFM development

Comparative study on the effect of alkali promoters (Li, Na, K) on the performance of **1%Ru/Al<sub>2</sub>O<sub>3</sub>** [Cimino et al. J. CO<sub>2</sub> Utilization 37 (2020)]



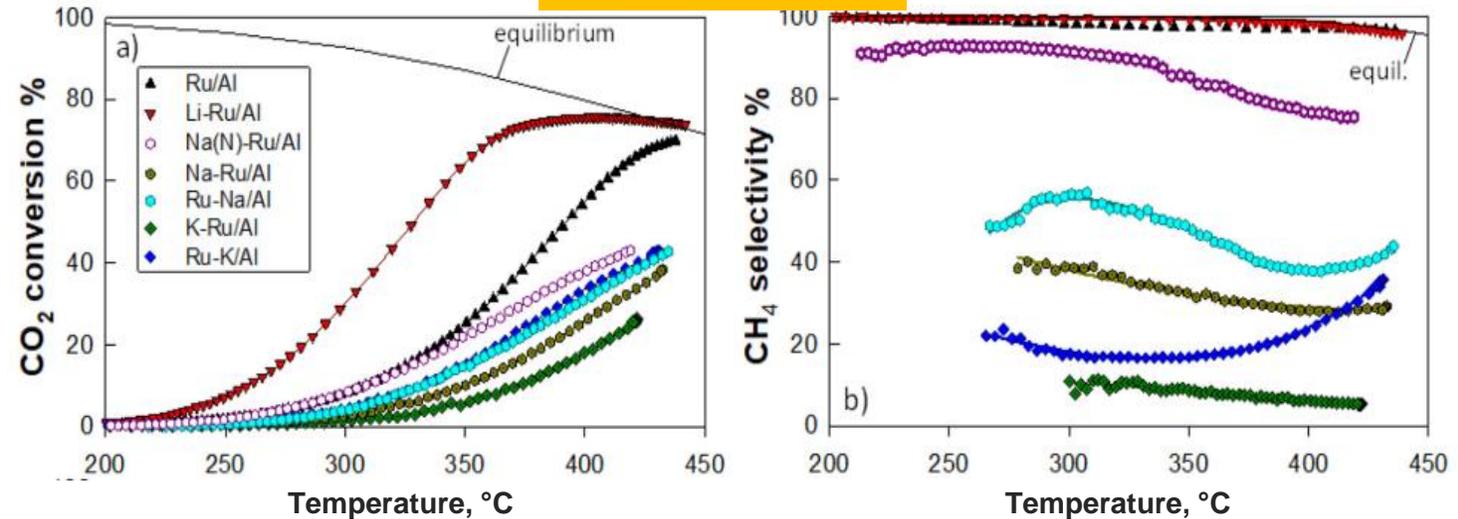
Catalyst	Alkali Precursor	Order of deposition	Alkali metal load (wt %)
Ru/Al	–	–	–
Li-Ru/Al	nitrate	1 <sup>st</sup> Ru, 2 <sup>nd</sup> alkali	1.73
Na(N)-Ru/Al	nitrate	1 <sup>st</sup> Ru, 2 <sup>nd</sup> alkali	4.34
Na-Ru/Al	carbonate	1 <sup>st</sup> Ru, 2 <sup>nd</sup> alkali	4.34
Ru-Na/Al	carbonate	1 <sup>st</sup> alkali, 2 <sup>nd</sup> Ru	4.34
K-Ru/Al	carbonate	1 <sup>st</sup> Ru, 2 <sup>nd</sup> alkali	5.66
Ru-K/Al	carbonate	1 <sup>st</sup> alkali, 2 <sup>nd</sup> Ru	5.66

## CO<sub>2</sub> TPD



Lithium: high CO<sub>2</sub> storage capacity,  
no formation of highly stable carbonates

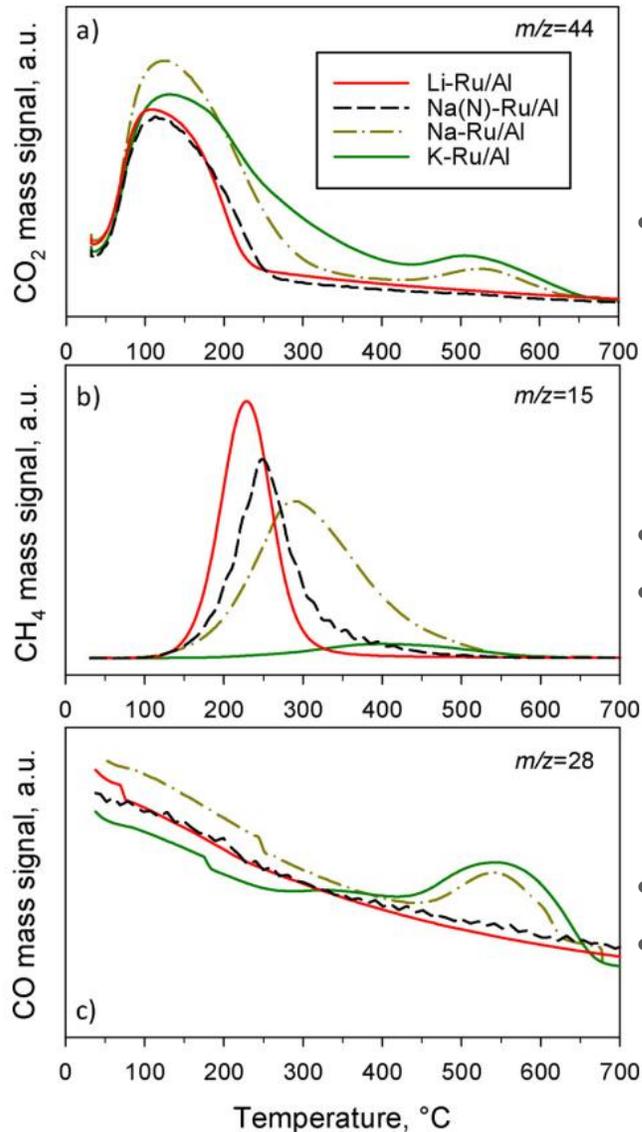
## Catalytic activity



Li - Ru synergy enhances Methanation  
Activity & Selectivity of Ru/Al<sub>2</sub>O<sub>3</sub>

# Key to success: DFM development

## H<sub>2</sub>-TPRx of pre-adsorbed CO<sub>2</sub>



- Pre-adsorbed CO<sub>2</sub> converted to CH<sub>4</sub> for T ≥ 130 °C

- Li-Ru has largest CH<sub>4</sub> formation at lowest T
- No residual CO<sub>2</sub> (full regeneration) @ 300 °C

- No CO formation with Li-Ru and Na(N)-Ru
- Absence of refractory carbonates

## Formation of **Li-Al mixed phases** lowers the stability of carbonates

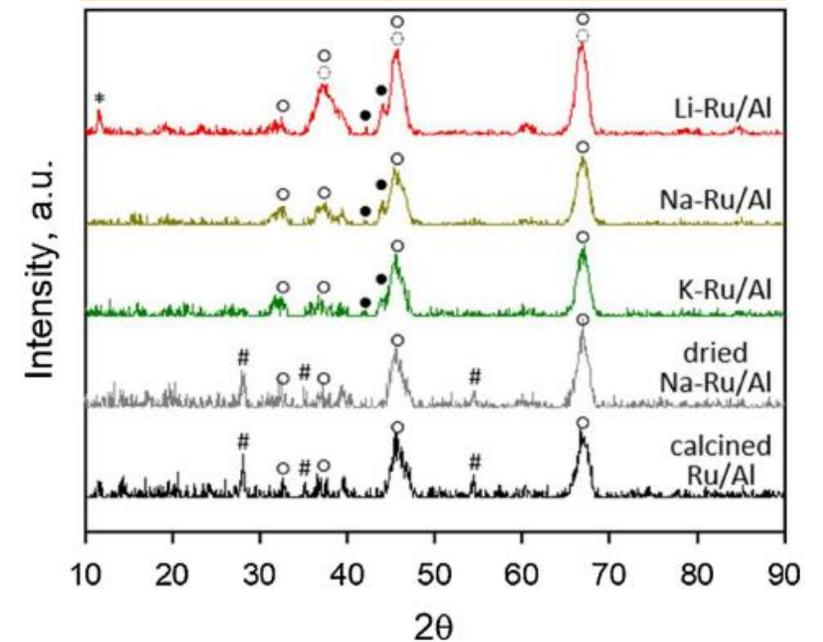
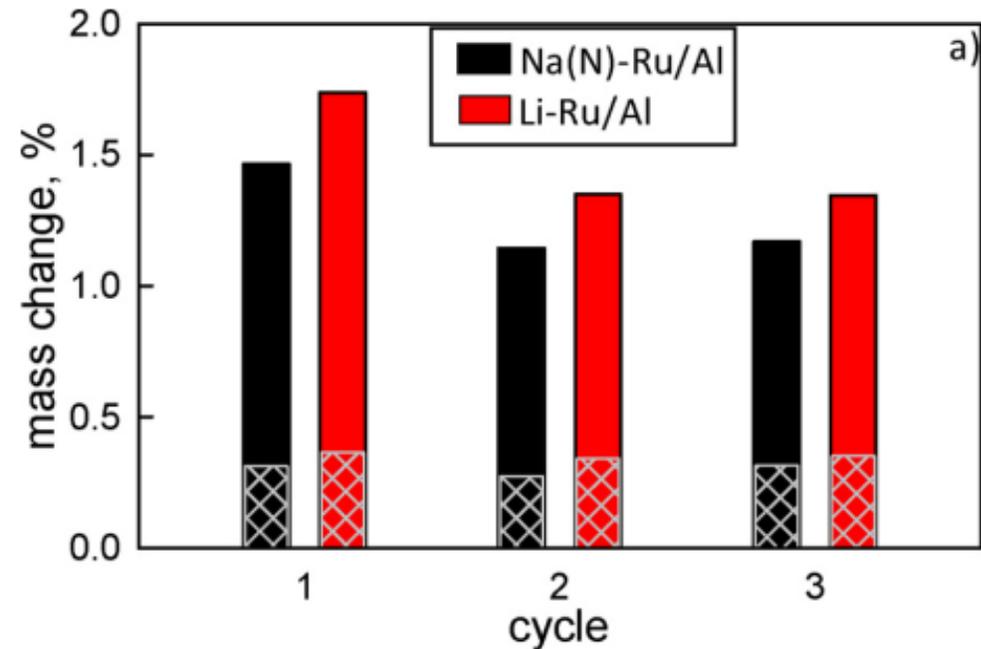
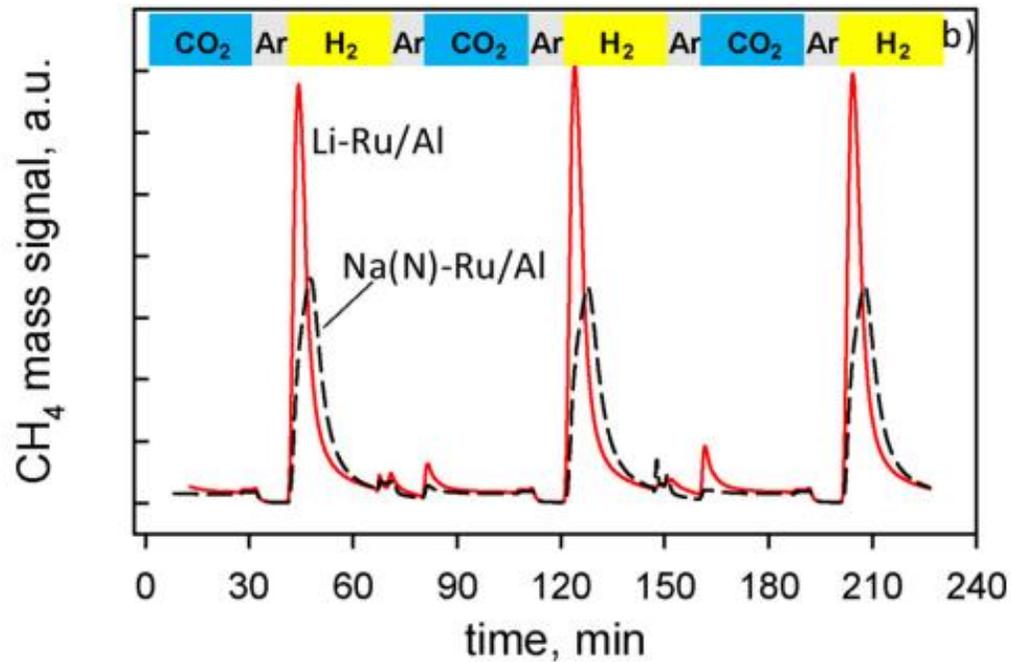


Fig. 2. XRD patterns of Li-Ru/Al, Na-Ru/Al and K-Ru/Al catalysts after testing in the CO<sub>2</sub> hydrogenation reaction. The spectra of dried Ru-/Al and Na-Ru/Al samples (before pre-reduction) are also reported for reference. Legend: ○ =  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> (PDF 29-63); □ = LiAl<sub>5</sub>O<sub>8</sub> (PDF 3-911); \* = Li<sub>2</sub>Al<sub>4</sub>(CO<sub>3</sub>)(OH) (PDF 37-185); ● = Ru (PDF 6-663); # = RuO<sub>2</sub> (PDF 43-1027).

# Key to success: DFM development

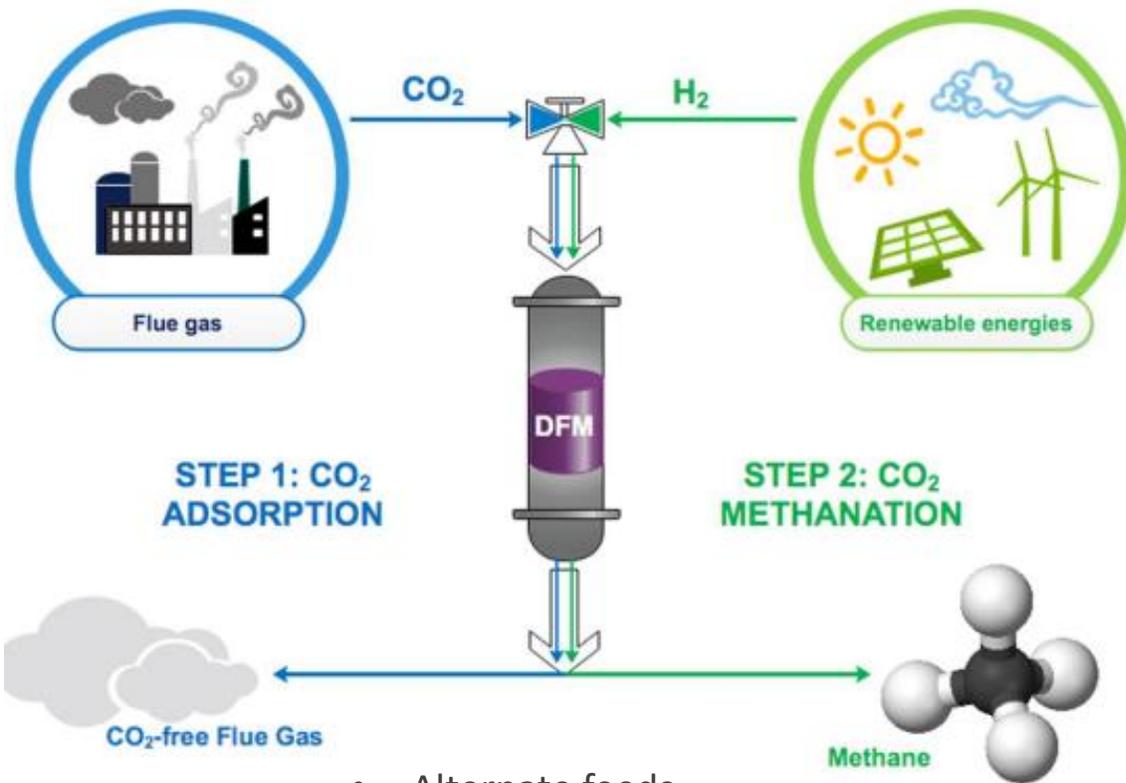
## Cyclic CO<sub>2</sub> capture and methanation (TG-MS @230 °C)



- Stable, repeatable CH<sub>4</sub> production already @ 230 °C
- Repeatable CO<sub>2</sub> capture (regeneration)
- Faster & larger CH<sub>4</sub> production over Li-Ru vs. Na-Ru
- Low Ru loading: remarkable CH<sub>4</sub> turnover (mol CH<sub>4</sub> / mol Ru)

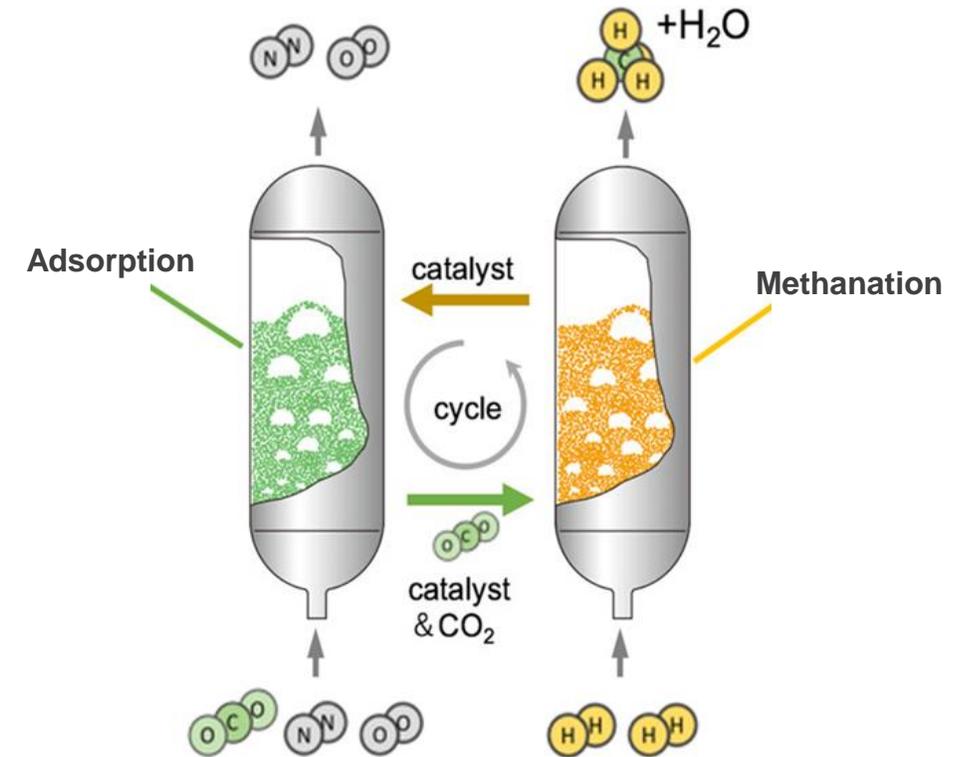
# Process intensification

## Single Fixed Bed Reactor



- Alternate feeds
- Intermediate purging
- Parallel reactors
- Isothermal operation
- Heat removal?

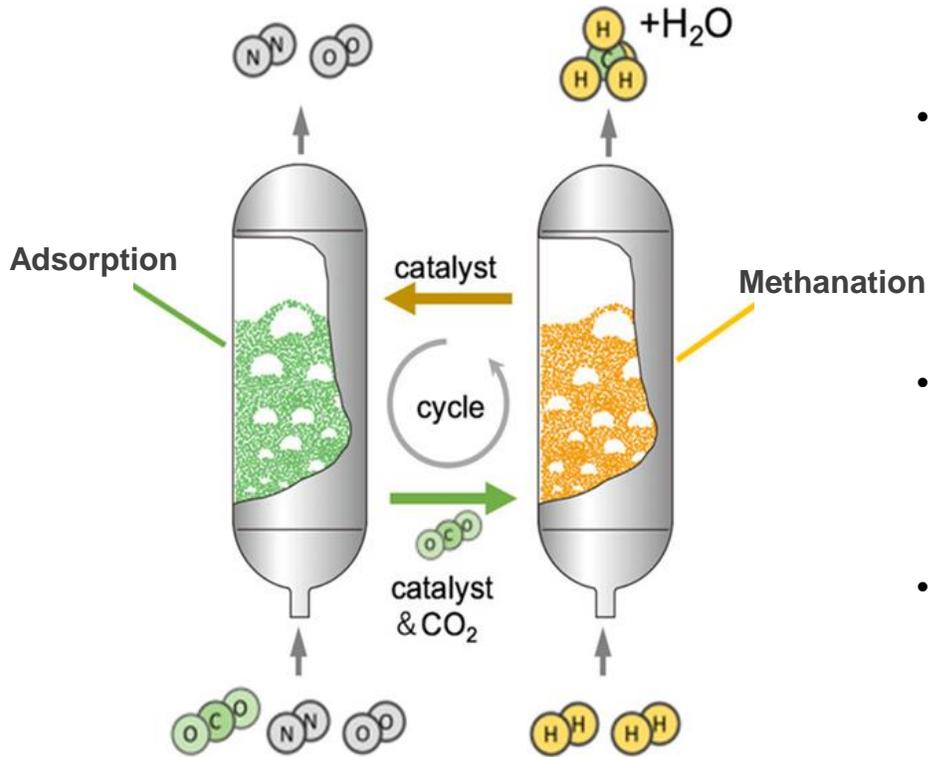
## Dual Interconnected Fluidized Bed Reactors



- Continuous operation
- Circulating DFM
- 2 reactors, optimized individually (i.e. different T)
- High heat transfer
- Mechanical stability / Attrition/ Fragmentation

# Project: ECO<sub>2</sub>Me

Efficient CO<sub>2</sub> capture and Methanation



- Develop highly innovative dual function catalytic materials to facilitate the production of methane from industrial flue gas emissions aiming at a significant increase in the overall efficiency compared to the State-of-the-Art: **Advanced Lithium Ceramics + Ru**
- Develop innovative, renewable energy driven, catalytic looping processes, to produce synthetic CH<sub>4</sub> demonstrating effectiveness and reduction of GHG emissions: **Dual Interconnected Fluidized Beds Technology**
- Address economic, regulatory, environmental and (critical) raw material constraints, as well as public acceptance issues and socio-economic impact related to the proposed technological pathway: Techno-Economic Evaluation (**TEE**), Life Cycle Assessment (**LCA**), Social Impact Assessment (**SIA**)